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# JAST (Journal of Animal Science and Technology) TITLE PAGE

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ARTICLE INFORMATION	Fill in information in each box below
<b>Article Type</b>	Research article
<b>Article Title (within 20 words without abbreviations)</b>	Characterization of sustainable bacterial cellulose of <i>Komagataeibacter rhaeticus</i> SLAM-JS1B isolated from Kombucha for biocontrol of Salmonella Typhimurium in animal production system
<b>Running Title (within 10 words)</b>	Antimicrobial property of BC of <i>K. rhaeticus</i> from Kombucha
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9 **Running head:** Antimicrobial property of BC of *K. rhaeticus* from Kombucha

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12 **Characterization of sustainable bacterial cellulose of *Komagataeibacter***

13 ***rhaeticus* SLAM-JS1B isolated from Kombucha for biocontrol of *Salmonella***

14 **Typhimurium in animal production system**

15

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32

33 **Abstract**

34

35 Bacterial cellulose (BC) is a high-purity, nanofibrillar biomaterial with considerable potential in the animal  
36 industry as both a functional dietary fiber and a carrier for bioactive compounds. In this study, three BC-  
37 producing *Komagataeibacter* strains were isolated from kombucha pellicles (*K. intermedius* SLAM-NK6B,  
38 *K. rhaeticus* SLAM-JS1B, and *K. rhaeticus* SLAM-JS2B), and their cellulose production under static  
39 conditions at 25°C was compared. The *K. rhaeticus* strains formed substantially thicker pellicles than *K.*  
40 *intermedius* with dry weight yields of  $120.8 \pm 28.3$  mg/L (SLAM-JS1B),  $113.3 \pm 15.0$  mg/L (SLAM-JS2B),  
41 and  $36.3 \pm 5.3$  mg/L (SLAM-NK6B), respectively. Leveraging the highest-yielding strain SLAM-JS1B, a  
42 sequential optimization strategy including one-variable-at-a-time (OVAT) screening, Plackett–Burman  
43 design (PBD), and Box–Behnken design (BBD) combined with response surface methodology, was  
44 employed to enhance BC production. Yeast extract, MgSO<sub>4</sub>, and ethanol were identified as key drivers. The  
45 optimized medium (10 g/L yeast extract, 2 g/L MgSO<sub>4</sub>, 10 mL/L ethanol, with glucose and KH<sub>2</sub>PO<sub>4</sub>  
46 maintained within the design-space ranges) yielded a cellulose titer of 2.795 g/L, representing a 37%  
47 increase relative to the baseline Saleh medium. Characterization by FT-IR and FE-SEM confirmed the  
48 structural, chemical, and morphological characteristics of BC, revealing a dense, highly porous nanofibrillar  
49 network. Furthermore, *Salmonella* Typhimurium–targeting phages were successfully immobilized on the  
50 BC matrix and retained lytic activity in antimicrobial assays. Collectively, our findings propose an  
51 optimized production platform for BC using *K. rhaeticus* SLAM-JS1B isolated from kombucha and  
52 highlight the functional utility of BC as a carrier for bioactives, underscoring its promise for pathogen  
53 biocontrol in animal production systems.

54 **Keywords:** *Komagataeibacter*, bacterial cellulose, nanofibrillar biomaterial, optimization production  
55 strategy, phage immobilization

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## 58 **Introduction**

59

60 Cellulose is one of the most abundant polysaccharides on Earth, produced by a diverse array of organisms  
61 including plants and microorganisms [1, 2]. Although plants serve as the primary natural source of cellulose  
62 in nature, its industrial extraction and purification are often complicated by the co-existence of lignin and  
63 hemicellulose, necessitating intensive chemical treatments such as alkaline pulping, acid hydrolysis, and  
64 bleaching [3]. In contrast, bacterial cellulose (BC) is synthesized extracellularly in a nanofibrillar form,  
65 inherently free of lignin and hemicellulose, and thus requires minimal downstream processing [4]. Owing  
66 to the absence of recalcitrant components, BC shows strong potential as an alternative fibrous feed source  
67 for herbivores, including ruminants [5-8]. In addition to its purity, BC exhibits a suite of advantageous  
68 physicochemical properties, including nanoscale fibrillar architecture, exceptional mechanical strength,  
69 high crystallinity, and remarkable water-holding capacity [9]. By coupling its nanoscale architecture with  
70 superior biocompatibility, BC functions as an effective carrier for hydrophilic compounds and a suitable  
71 vehicle for targeted antimicrobial delivery in animal health applications. In this context, BC-based  
72 antimicrobial delivery strategies show great potential against representative feedborne pathogens of major  
73 economic concern in livestock industries, such as *Salmonella enterica* serovar Typhimurium (*S.*  
74 Typhimurium) [14-16]. Despite its considerable potential, however, the inherently low yield and slow  
75 productivity of BC represent significant barriers to its commercial feasibility [17]. These limitations  
76 underscore the need for advanced bioprocess optimization strategies to improve production efficiency and  
77 support the scalable application of BC across diverse industries.

78 The genus *Komagataeibacter* is widely recognized as one of the most prominent bacterial producers of  
79 cellulose, with numerous strains reported to achieve high yield capabilities [18]. The composition of the  
80 culture medium, particularly the types of carbon and nitrogen sources, directly affects microbial metabolism  
81 and the biosynthetic pathways involved in BC production [19]. Although most *Komagataeibacter* species  
82 require substantial nitrogen supplementation to achieve efficient cellulose biosynthesis, *K. rhaeticus* has  
83 recently garnered attention as a promising producer due to its capacity to maintain relatively high BC yields

84 even under nitrogen-limited conditions [20, 21]. The Hestrin–Schramm (HS) medium, one of the most  
85 widely used formulations for BC production, contains glucose (20 g/L) as the carbon source and peptone  
86 (5 g/L) together with yeast extract (5 g/L) as nitrogen sources [22, 23]. Notably, significant cost differences  
87 among these components have been reported, with glucose priced at approximately \$0.70/kg, yeast extract  
88 at \$1.70/kg, and peptone at \$6.17/kg [24]. Consequently, nitrogen sources are a major cost driver in bacterial  
89 culture media for large-scale BC production. The intrinsic ability of *K. rhaeticus* to sustain high BC yields  
90 under reduced nitrogen input therefore confers a notable economic advantage. [20]. Although *K. rhaeticus*  
91 represents significant industrial potential, studies on the optimization of its BC production are still limited.  
92 A systematic investigation of strain-specific factors, including nutrient composition, additive  
93 supplementation, and physicochemical cultivation conditions, is essential to fully harness its potential as an  
94 efficient biocatalyst for BC synthesis.

95 In recent years, medium optimization for the production of microbially derived biomaterials has  
96 advanced markedly with the adoption of statistical methodologies, enhancing process efficiency, shortening  
97 experimental timelines, and reducing labor costs, thereby improving overall process economics. Strategic  
98 implementation of design-of-experiments approaches can substantially reduce the number of trials required  
99 for robust process optimization. For instance, a one-variable-at-a-time (OVAT) method was employed to  
100 investigate essential nutrient factors in the culture medium [25, 26]. The Plackett–Burman design (PBD)  
101 has proven highly effective for the preliminary screening of medium components, enabling the  
102 identification of significant variables with a minimal number of experimental runs [27]. While PBD is  
103 widely adopted for the initial optimization steps in fermentation processes, its limitation lies in the inability  
104 to evaluate interaction effects among variables. To address this limitation, the Box–Behnken design (BBD)  
105 offers a powerful follow-up approach, enabling the exploration of variable interactions and the development  
106 of predictive mathematical models for microbial productivity [28, 29].

107 In this study, we isolated *K. rhaeticus* SLAM-JS1B, a high-yielding BC-producing strain, from  
108 kombucha pellicles. Then, a three-step empirical, sequential statistical approach, including OVAT (for  
109 initial screening of nutrient preferences), PBD (for identifying key medium components), and BBD (for

110 analyzing interactions and defining optimal conditions), was employed to systematically optimize BC  
111 production. This sequential optimization framework significantly enhanced BC yield, improved process  
112 reproducibility, and enabled scalability for industrial application. Moreover, optimized cultivation of *K.*  
113 *rhaeticus* SLAM-JS1B yielded BC with characteristic nanofibrillar architecture, high water-holding  
114 capacity, and robust mechanical strength. These structural and physicochemical features also facilitated the  
115 effective immobilization of phages, supporting their potential utility as a bioactive delivery matrix [30].  
116 Collectively, this work highlights the dual advantage of *K. rhaeticus*-derived BC as both a cost-effective  
117 biomaterial and a versatile platform for functional delivery applications in the animal industry.

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## 119 **Materials and methods**

120

### 121 **Isolation of bacterial cellulose (BC) producing strain**

122 A kombucha starter culture maintained in our laboratory (Seoul National University, Seoul, South Korea)  
123 was used to isolate BC-producing strains. The starter was prepared by infusing green tea (Dongsuh, South  
124 Korea) into an 8% (w/v) cane sugar solution (United Farmer & Industry, Thailand) for 10 min, followed by  
125 sterilization by autoclaving, as described previously [31]. The culture was incubated under static, aerobic  
126 conditions at 25 °C for 20 days. Following incubation, the cellulose pellicle formed at the air–liquid  
127 interface was harvested and homogenized by blending it with an equal volume of 0.85% (w/v) saline using  
128 a commercial blender (HR3757, Philips, Netherlands). The resulting suspension was serially diluted and  
129 plated on MRS agar to isolate BC-producing strains. Using this procedure, *Komagataeibacter intermedius*  
130 SLAM-NK6B, *K. rhaeticus* SLAM-JS1B, and *K. rhaeticus* SLAM-JS2B were isolated [31]. Whole-  
131 genome sequencing of the isolates was performed, and the complete genome sequences have been deposited  
132 in GenBank under the following accession numbers: *K. intermedius* SLAM-NK6B (CP185240.1) and *K.*  
133 *rhaeticus* SLAM-JS1B (CP186559.1). The 16S rRNA gene sequence of *K. rhaeticus* SLAM-JS2B has also  
134 been deposited under the accession number (PX485042). Genomic analysis followed a previously  
135 established pipeline [32-35]. Long-read sequencing was conducted on the Oxford Nanopore MinION Mk1B  
136 platform (R10). The resulting reads were assessed using NanoPlot (v1.42.0), yielding 285,680 reads (mean  
137 read length, 9,327 bp; mean read quality, 18.5) and totaling 2,664,573,670 bp (~2.66 Gb). Assembly of the  
138 Nanopore reads resulted in a complete genome of 2,569,831 bp and a GC content of 62.85%. Annotation  
139 using the NCBI Prokaryotic Genome Annotation Pipeline predicted 2,520 protein-coding genes, 9 rRNA  
140 operons, and 58 tRNA genes. Orthologous Average Nucleotide Identity analysis showed the highest identity  
141 (99.48%) to the type strain, *K. rhaeticus* LMG 22126 [36].

142

### 143 **Preparation of BC**

144 BC was produced using *K. rhaeticus* SLAM-JS1B, previously isolated from kombucha pellicles. All  
145 reagents were purchased from Sigma-Aldrich (St. Louis, MO, USA) unless otherwise stated. The isolated  
146 strain was stored at  $-80\text{ }^{\circ}\text{C}$  and subsequently cultured on modified Yamanaka medium containing 1.5%  
147 (w/v) D-glucose, 1.5% (w/v) yeast extract, 0.1% (w/v)  $\text{KH}_2\text{PO}_4$ , 0.1% (w/v)  $\text{MgSO}_4$ , 7 mL/L ethanol, and  
148 1.5% (w/v) agar (pH 7.2) [4]. Plates were incubated at  $25\text{ }^{\circ}\text{C}$  for 3 days. A single colony was selected and  
149 inoculated into 3 mL of Yamanaka liquid medium in round-bottom test tubes (Falcon, Corning), then  
150 incubated at  $25\text{ }^{\circ}\text{C}$  for 3 days. Subsequently, 2 mL of the culture supernatant was transferred into 100 mL  
151 of Yamanaka liquid medium and incubated statically at  $25\text{ }^{\circ}\text{C}$  for 14 days.

152 After incubation, the BC pellicle was separated from the culture broth. The culture supernatant was  
153 filtered through a  $0.2\text{-}\mu\text{m}$  pore-size polyvinylidene fluoride (PVDF) syringe filter (Whatman, Maidstone,  
154 UK) and stored at  $4\text{ }^{\circ}\text{C}$  until use. The harvested BC pellicles were treated with 0.5% NaOH at  $90\text{ }^{\circ}\text{C}$  for 30  
155 min to remove bacterial cells and residual impurities, followed by repeated washing with distilled water  
156 ( $\text{dH}_2\text{O}$ ) until neutral pH was reached [37]. The purified BC was freeze-dried to constant weight using a  
157 freeze dryer (Operon, Gyeonggi, South Korea). The final BC concentration was determined gravimetrically  
158 and expressed as grams per liter (g/L).

159

## 160 **Optimization of BC production**

### 161 **One Variable at a Time (OVAT) Screening**

162 To identify the most suitable basal medium for BC production by *K. rhaeticus* SLAM-JS1B, several  
163 standard BC media were first evaluated: Hestrin–Schramm medium (HS), modified HS medium (mHS),  
164 modified Yamanaka medium (MYM), modified glucose–yeast extract medium (GYM), and Saleh medium  
165 (SM) [4, 38-40]. The medium that supported the highest BC yield was selected as the basal medium for  
166 subsequent experiments. To assess the effects of different carbon and nitrogen sources on BC production,  
167 the OVAT method was employed. Various carbon sources, including glucose, sucrose, lactose, glycerol,  
168 sorbitol, and mannitol, were tested in the basal medium at a concentration of 1.5% (w/v). In parallel, several  
169 organic and inorganic nitrogen sources were evaluated in the basal medium at 1.3% (w/v), including yeast

170 extract, peptone, tryptone, ammonium nitrate, ammonium chloride, and ammonium sulfate. All  
171 fermentation experiments were carried out in 250 mL Erlenmeyer flasks containing 100 mL of sterile basal  
172 production medium. Cultures were incubated under static conditions at the specified temperature. Each  
173 condition was tested in triplicate to ensure reproducibility and statistical reliability of the results.

174

### 175 **Plackett–Burman Design (PBD)**

176 PBD was employed to evaluate the influence of various nutritional and physical parameters on BC  
177 production [27]. In this study, six independent variables were evaluated: glucose ( $X_1$ ), yeast extract ( $X_2$ ),  
178  $\text{KH}_2\text{PO}_4$  ( $X_3$ ),  $\text{MgSO}_4$  ( $X_4$ ), ethanol ( $X_5$ ), and incubation time ( $X_6$ ). These variables were assessed across  
179 12 experimental runs based on the PBD matrix, along with two additional center-point replicates to validate  
180 the model's accuracy. All experiments were conducted in triplicate to ensure statistical reliability. Each  
181 factor was tested at two levels, coded as +1 (high) and -1 (low). BC production (g/L) was used as the  
182 response variable. Table 1 summarizes the experimental design: each row represents an individual trial, and  
183 each column corresponds to a specific factor.

184 The experimental results were fitted to a first-order polynomial model, as shown in Equation (1):

$$185 \quad Y = \beta_0 + \sum \beta_i X_i$$

187 where  $Y$  denotes the predicted BC production (g/L),  $\beta_0$  is the model intercept,  $\beta_i$  is the estimated  
188 coefficient for each independent variable, and  $X_i$  is the coded level of the respective factor.

190 The statistical significance of each factor was assessed using regression analysis, including p-value  
191 calculations to evaluate each parameter's contribution to BC yield. All fermentation experiments were  
192 conducted in 250-mL Erlenmeyer flasks containing 100 mL of the respective media, formulated according  
193 to the PBD matrix.

194

### 195 **Box-Behnken Design (BBD)**

196 The most significant variables identified from the PBD were further optimized using a three-level BBD  
197 to determine the optimal conditions for maximum BC production [28, 29]. The application of BBD involved  
198 three primary steps: conducting statistically designed experiments, analyzing the experimental outcomes to  
199 model the predicted response, and validating the adequacy of the developed model.

200 Thirteen BBD runs were performed according to the design matrix, together with two center-point  
201 replicates (15 runs in total), to evaluate both the individual and interaction effects of the three key variables  
202 identified through PBD. These variables were yeast extract ( $X_1$ ),  $MgSO_4$  ( $X_2$ ), and ethanol ( $X_3$ ). Each factor  
203 was tested at three coded levels:  $-1$  (low),  $0$  (center), and  $+1$  (high), with  $0$  representing the mid-point of  
204 each experimental range (Table 2). All other medium components and cultivation parameters were  
205 maintained at their previously determined effective levels, classified as either high or low according to the  
206 regression analysis of the PBD results. A second-order (quadratic) polynomial model was employed to  
207 predict BC yield ( $Y$ ) based on the interactions among the independent variables ( $X_1$ ,  $X_2$ , and  $X_3$ ).

208 The general form of the model is presented in Equation (2):

209  
210 
$$Y = \beta_0 + \beta_1 X_1 + \beta_2 X_2 + \beta_3 X_3 + \beta_{12} X_1 X_2 + \beta_{13} X_1 X_3 + \beta_{23} X_2 X_3 + \beta_{11} X_1^2 + \beta_{22} X_2^2 + \beta_{33} X_3^2$$

211 where  $Y$  is the predicted response (BC yield, g/L);  $\beta_0$  is the intercept,  $\beta_1$ ,  $\beta_2$ , and  $\beta_3$  are the linear  
212 coefficients;  $\beta_{12}$ ,  $\beta_{13}$ , and  $\beta_{23}$  are the interaction coefficients; and  $\beta_{11}$ ,  $\beta_{22}$ , and  $\beta_{33}$  are the quadratic  
213 coefficients. The optimal values of the independent variables were estimated by taking the partial  
214 derivatives of the polynomial equation and setting them to zero. All experimental trials were conducted in  
215 triplicate to ensure reproducibility and statistical reliability.

217

## 218 **Structural and physicochemical analysis of BC by Fourier-transform infrared (FT-IR) spectroscopy**

219 Freeze-dried BC samples were analyzed by FT-IR spectroscopy and compared with a standard cellulose  
220 reference. Spectra were acquired with a Nicolet 6700 FT-IR spectrometer (Thermo Fisher Scientific,  
221 Waltham, MA, USA) in the  $4000\text{--}500\text{ cm}^{-1}$  range, using a resolution of  $8\text{ cm}^{-1}$  and 32 scans per sample.

222

223 **Morphological analysis of BC by Field Emission-Scanning Electron Microscopy (FE-SEM)**

224 The surface morphology of BC membranes was examined via FE-SEM (SIGMA, Carl Zeiss, Germany)  
225 operated at an accelerating voltage of 5 kV. The instrument provided a resolution of 1.0 nm with an emission  
226 voltage of 1.5 kV. Samples were sputter-coated with platinum to minimize charging and improve  
227 conductivity. High-resolution images were acquired at 100,000× magnification to assess the nanofibrillar  
228 architecture of BC.

229

230 **Phage propagation and lysate preparation**

231 *Salmonella enterica* serovar Typhimurium ST1, a pig-derived host strain (KVCC-BA2000161), was  
232 cultured overnight in tryptic soy broth (TSB; BD, Sparks, MD, USA) at 37°C with shaking at 160 rpm [41].  
233 To amplify SLAM\_phiST1N3, lytic phage in the *Cornellvirus* genus for biocontrol of a multidrug-resistant  
234 *S. Typhimurium* in the swine industry chain, 1 mL of the overnight bacterial culture was mixed with 20 mL  
235 of fresh TSB and 20 mL of phage-containing supernatant [42]. The mixture was incubated for more than  
236 16 h at 37 °C with shaking at 160 rpm to allow phage propagation. After incubation, cultures were  
237 centrifuged at 8,000 rpm for 15 min to remove bacterial cells. The resulting supernatant was collected,  
238 passed through a 0.22 µm pore-size syringe filter (Whatman, Maidstone, England), and used as the crude  
239 phage lysate. Phage purification was performed through repeated plaque isolation and elution, followed by  
240 final sterilization by filtration. The purified lysate was used as working phage stock for all subsequent  
241 experiments.

242

243 **Phage adsorption onto BC membranes**

244 The phage lysate was buffer-exchanged into PBS (pH 7.4) and diluted to  $1 \times 10^8$  PFU/mL for subsequent  
245 immobilization assays. SLAM\_phiST1N3 was immobilized onto BC pellicles by physical adsorption [43].  
246 Purified BC membranes were submerged in the phage suspension and incubated at room temperature on a  
247 tilting shaker (LaboShaker R100, Gyrozen, South Korea) at 10 rpm for 1 h. After incubation at room

248 temperature, membranes were rinsed with ultrapure distilled water (10977-023, Invitrogen, USA) to remove  
249 non-adsorbed phages. BC-bound phages were used immediately in antimicrobial assays [10].

250

### 251 **Antimicrobial activity on solid media**

252 *S. Typhimurium* ST1 was cultured in tryptic soy broth (TSB; BD, Sparks, MD, USA) at 37 °C with shaking  
253 at 160 rpm to prepare an indicator suspension ( $\sim 10^8$  CFU/mL) [42]. For the overlay, soft agar (0.75% w/v)  
254 was prepared by mixing the bacterial suspension with tryptic soy agar (TSA; 1.5% w/v agar) and overlaying  
255 onto solidified TSA plates to form a uniform bacterial lawn. The BC films (approximately 10 × 10 mm)  
256 with or without adsorbed phages were aseptically placed onto the agar surface using the spot diffusion  
257 method. After incubation at 37°C for 24 h, antimicrobial activity was evaluated by measuring zones of  
258 inhibition around BC samples.

259

### 260 **Liquid inhibition assay**

261 For liquid-phase inhibition, an ST1 culture was grown to  $OD_{600} \approx 0.30$  (mid-log; approximately  $10^8$   
262 CFU/mL), then diluted to approximately  $10^6$  CFU/mL in fresh TSB. A 96-well plate assay was set up with  
263 180  $\mu$ L TSB, 10  $\mu$ L bacterial suspension, and 10 mg of either phage-loaded or control BC per well (final  
264 volume 200  $\mu$ L). Plates were incubated at 37 °C with orbital shaking, and bacterial growth was monitored  
265 every hour for 14 h by measuring  $OD_{600}$  using a microplate reader. All experiments were conducted in  
266 triplicate.

267

### 268 **Statistical analysis**

269 Statistical analysis for the OVAT experiments was conducted using unpaired two-tailed t-tests, and p-  
270 values  $< 0.05$  (\*),  $< 0.01$  (\*\*),  $< 0.001$  (\*\*\*), and  $< 0.0001$  (\*\*\*\*) were considered statistically significant.  
271 All values are presented as the mean  $\pm$  standard deviation (SD) and were obtained from three or more  
272 independent experiments. Statistical analyses, including regression modeling, analysis of variance  
273 (ANOVA), and model adequacy evaluations ( $R^2$ , adjusted  $R^2$ , and p-values), were conducted using Minitab

274 statistical software (Minitab, LLC, State College, PA, USA). Optimization of the significant variables was  
275 conducted using Microsoft Excel Solver to support predictive modeling and model validation.  
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277 **Results**

278

279 **Isolation and identification of BC producing strains from Kombucha**

280 Three bacterial strains including *K. intermedius* SLAM-NK6B, *K. rhaeticus* SLAM-JS1B, and *K.*  
281 *rhaeticus* SLAM-JS2B, were successfully isolated from kombucha pellicles and assessed for BC production  
282 under static aerobic conditions at 25 °C in GYM medium (Fig. 1A). The *K. rhaeticus* strains consistently  
283 exhibited more pronounced pellicle formation compared to *K. intermedius*. Whole-genome analysis of *K.*  
284 *intermedius* SLAM-NK6B revealed a canonical BC biosynthetic gene cluster (*bcsA–bcsB–bcsC*) at  
285 positions 3,165,943–3,174,574, along with an additional, frameshifted copy of *bcsC* located between  
286 positions 1,737,762 – 1,746,004 (Fig. 1B). Interestingly, genomic characterization of *K. rhaeticus* SLAM-  
287 JS1B indicated a *bcs* locus comprising *bcsB* and *bcsC*, with a putative glycosyltransferase family 2 (GT2)  
288 gene (Fig. 1C). Quantification of freeze-dried pellicles revealed that *K. intermedius* SLAM-NK6B produced  
289  $36.3 \pm 5.3$  mg/L of BC, while *K. rhaeticus* SLAM-JS1B and SLAM-JS2B yielded  $120.8 \pm 28.3$  mg/L and  
290  $113.3 \pm 15.0$  mg/L, respectively (Fig. 1D). Among them, *K. rhaeticus* SLAM-JS1B demonstrated the  
291 highest productivity and was therefore selected as the representative BC producing strain for subsequent  
292 optimization experiments.

293

294 **Optimization of BC production using three-step sequential and statistical approaches**

295 **1) OVAT screening**

296 To determine the most suitable basal medium for subsequent optimization, five standard formulations  
297 were evaluated under static conditions. Among them, SM supported the highest BC production (2.045 g/L),  
298 yielding approximately 9% more than the second-best medium, MYM (1.870 g/L). BC yields from MHSM  
299 (1.388 g/L), HSM (1.158 g/L), and GYM (0.722 g/L) decreased in the following order: MHSM > HSM >  
300 GYM (Fig. 2A). The BC yield with SM was significantly higher than those with HSM and GYM ( $p = 0.041$   
301 and 0.003, respectively). A similar trend was observed for both BC yield and productivity. SM also showed  
302 the highest productivity (26%), further supporting its selection as the basal medium. Next, to assess the

303 influence of different carbon sources on BC production, the original carbon source in SM (glucose) was  
304 replaced with various alternatives at a concentration of 1.5%, following the OVAT approach. While all  
305 tested carbon sources supported BC production, glucose yielded the highest BC concentration (1.988 g/L),  
306 as shown in Fig. 2B. The remaining carbon sources ranked as follows: mannitol (1.925 g/L) > sucrose  
307 (1.647 g/L) > glycerol (1.539 g/L) > sorbitol (1.109 g/L) > lactose (0.694 g/L). In addition, various organic  
308 and inorganic nitrogen sources were evaluated at 1.3% (w/v) to assess their effects on BC production  
309 (Figure 2C). Among these, yeast extract supported the highest BC production (1.820 g/L), followed by  
310 peptone (1.640 g/L), tryptone (1.475 g/L), ammonium chloride (0.474 g/L), and ammonium nitrate (0.162  
311 g/L). Notably, ammonium sulfate did not support BC production. Finally, incubation temperature was  
312 varied to identify the optimal thermal condition for BC synthesis. The highest yield was achieved at 25°C  
313 (1.926 g/L), followed by 20°C (1.758 g/L) and 30°C (1.039 g/L) (Fig. 2D). No detectable BC was produced  
314 at 15°C or 35°C, underscoring the temperature sensitivity of the strain.

315

## 316 **2) PBD for variable screening**

317 Based on the results of the OVAT experiments, a PBD was employed to evaluate the influence of six  
318 independent nutritional and physical variables on BC production through 12 experimental runs. Each  
319 variable was evaluated at two levels, coded as high (+1) and low (-1), and BC yield (g/L) served as the  
320 response (Table 1). The main effects analysis revealed that glucose, magnesium sulfate, ethanol, and  
321 incubation time exerted positive effects on BC production, whereas yeast extract and potassium phosphate  
322 ( $\text{KH}_2\text{PO}_4$ ) had negative effects (Fig. 3A). Among the tested variables, ethanol, magnesium sulfate, and  
323 yeast extract were identified as the most significant factors influencing BC production, as confirmed by the  
324 Pareto chart (Fig. 3B). These three variables were statistically significant within the model. As the PBD  
325 relies on a first-order linear model, regression analysis yielded the following predictive equation:

326

327 Eq. 1: Result = 0.659 + 0.01264( $X_1$ ) - 0.02233( $X_2$ ) - 0.0257( $X_3$ ) + 0.2960( $X_4$ ) + 0.14329( $X_5$ ) + 0.00644( $X_6$ )

328

329 The model exhibited a high degree of fit, with an  $R^2$  value of 0.968 and an adjusted  $R^2$  (adj- $R^2$ ) of 0.962,  
330 indicating strong predictive accuracy and reliability of the applied model.

331

### 332 **3) BBD for optimized conditions**

333 The most significant variables identified from the PBD, namely yeast extract ( $X_1$ ),  $MgSO_4$  ( $X_2$ ), and  
334 ethanol ( $X_3$ ), were further investigated using a three-level BBD to determine the optimal concentrations for  
335 maximizing BC production (Table 2). According to the regression analysis, increasing concentrations of  
336  $MgSO_4$  and ethanol had a positive effect on BC yield, whereas higher levels of yeast extract negatively  
337 influenced BC production. The interaction effects between variables on BC yield were visualized using  
338 three-dimensional surface plots (Fig. 4A, 4B, and 4C). In these plots, two independent variables were  
339 represented on the X- and Y-axes, while BC yield was plotted on the Z-axis. The third variable was held  
340 constant at its midpoint value. The regression equation derived from the BBD for predicting BC production  
341 as a second-order polynomial model is as follows:

342

343 Eq. 2: Result =  $0.570 - 0.0254(X_1) - 0.1535(X_2) + 0.0751(X_3) + 0.001093(X_1)^2 + 0.0871(X_2)^2 +$   
344  $0.003053(X_3)^2 - 0.00388(X_1X_2) - 0.003070(X_1X_3) + 0.02466(X_2X_3)$

345

346 The BBD model demonstrated a high level of fit, with an  $R^2$  value of 0.968 and an adjusted  $R^2$  of 0.960,  
347 indicating good reliability and predictive capability. Using Excel's Solver function to predict the optimal  
348 conditions for maximal BC production, the best combination was determined to be 10 g/L of yeast extract,  
349 2 g/L of  $MgSO_4$ , and 10 mL/L of ethanol, resulting in a predicted BC yield of 2.584 g/L. This optimized  
350 yield was 1.26 times higher than that obtained using the original Saleh medium formulation. Experimental  
351 validation of the optimized model yielded an actual BC production of 2.795 g/L, demonstrating a prediction  
352 accuracy of 92%. Overall, the final optimized medium formulation resulted in approximately a 37%  
353 improvement in BC productivity compared to the baseline SM. This result suggests the effectiveness of the  
354 multi-step optimization strategy in enhancing BC yield and process efficiency.

355

356 **Physicochemical and morphological characterization of BC from *K. rhaeticus* SLAM-JS1B**

357 The FT-IR spectrum of freeze-dried BC was compared with that of microcrystalline cellulose (MCC) as  
358 a reference (Fig. 5A). Both BC and MCC exhibited characteristic absorption bands at 3340 cm<sup>-1</sup> (O–H  
359 stretching), 2900 cm<sup>-1</sup> (C–H stretching), 1430 cm<sup>-1</sup> (CH<sub>2</sub> bending), and 1060 cm<sup>-1</sup> (C–O–C stretching) [44,  
360 45]. The similarity of the spectral patterns confirms the polysaccharide nature of the produced BC and its  
361 structural consistency with native cellulose. The physiological and morphological features of BC were  
362 further analyzed by FE-SEM (Fig. 5B). The micrographs revealed a dense and interconnected nanofibrillar  
363 network with a highly porous architecture. The fibers were randomly oriented and extensively entangled,  
364 forming a mesh-like structure typical of microbial cellulose. This nanoarchitecture offers a large surface  
365 area and open porosity, providing favorable conditions for functionalization and biomolecule  
366 immobilization.

367  
368 **Phage immobilized BC and antimicrobial activity against *S. Typhimurium***

369 Given the porous and highly entangled nanofibrillar structure, the BC matrix was investigated as a  
370 potential carrier for phage delivery. SEM imaging of phage-loaded BC confirmed the successful adsorption  
371 of *S. Typhimurium* ST1 phages onto cellulose fibrils, with distinct phage particles clearly visualized on the  
372 nanofiber surfaces (Fig. 6A and 6B). The phages were found to be immobilized and entrapped within the  
373 BC at a level of  $5.8 \pm 0.3$  log particles/mm<sup>2</sup> (Fig. 6C). The antimicrobial efficacy of phage immobilized BC  
374 (phage–BC) phagewas evaluated using a lawn inhibition assay. While native BC exerted no detectable  
375 inhibitory effect against *S. Typhimurium* (Fig. 6D), BC samples immobilized with SLAM\_phiST1N3 lytic  
376 phage produced clear inhibition zones, confirming the retained infectivity and lytic capacity of the  
377 entrapped phages (Fig. 6E). In broth, phage–BC markedly suppressed the growth of *S. Typhimurium* ST1  
378 during the early phase of incubation relative to the control (Fig. 6F). Specifically, OD<sub>600</sub> remained near  
379 baseline for approximately 2 h and increased only modestly thereafter, reaching  $0.248 \pm 0.014$  at 4 h,  
380 compared to  $0.620 \pm 0.006$  in the untreated control ( $p < 0.05$ ). The time to reach OD<sub>600</sub> = 0.5 was delayed by

381 approximately 3 h in the phage-treated group, indicating a pronounced early antibacterial effect. Between  
382 6 and 10 h, bacterial growth resumed, and OD<sub>600</sub> values approached those of the control group by 10–12 h,  
383 reflecting partial regrowth after phage-induced lysis. Integrated growth (AUC<sub>0-6h</sub>) was reduced by 56.8%  
384 in the BC-treated group compared with the control (2.805 vs. 1.211 OD·h; trapezoidal rule on hourly OD<sub>600</sub>  
385 means).  
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## 387 Discussion

388

389 In this study, we established a stepwise, statistically grounded optimization strategy combining OVAT,  
390 PBD, and BBD to enhance BC production by *K. rhaeticus* SLAM-JS1B. Using Saleh medium as the  
391 baseline reference, initial screening identified glucose and yeast extract as effective carbon and nitrogen  
392 sources, respectively, and indicated 25 °C as the optimal cultivation temperature under static conditions.  
393 Building on these insights, PBD highlighted ethanol, MgSO<sub>4</sub>, and yeast extract as the principal variables  
394 affecting BC yield, and subsequent BBD quantified their individual and interactive effects. The final  
395 optimized formulation consisted of 10 g/L yeast extract, 2 g/L MgSO<sub>4</sub>, and 10 mL/L ethanol, with glucose  
396 and KH<sub>2</sub>PO<sub>4</sub> maintained at their design-space levels. This recipe yielded an experimentally validated BC  
397 yield of 2.795 g/L, representing approximately a 37% improvement over the baseline. Notably, the  
398 optimized formulation reduced nitrogen input while enhancing productivity, offering both economic and  
399 environmental advantages. Although *K. intermedius* SLAM-NK6B also produced BC, *K. rhaeticus* SLAM-  
400 JS1B demonstrated superior yield and consistency under identical conditions.

401 We therefore designated *K. rhaeticus* SLAM-JS1B as the primary experimental strain and implemented  
402 a stepwise optimization strategy to enhance BC production. A notable outcome of the screening and  
403 modeling sequence was the asymmetric role of nitrogen: moderate levels of yeast extract supported robust  
404 production, whereas concentrations exceeding the optimum were associated with reduced yields. This  
405 pattern is consistent with a metabolic shift toward biomass accumulation rather than BC synthesis when  
406 nitrogen is in excess [46]. By contrast, ethanol and MgSO<sub>4</sub> exerted positive, dose-dependent effects on BC  
407 production. The stimulatory response to ethanol is consistent with prior observations that ethanol can  
408 modulate carbon flux toward UDP-glucose-dependent routes and suppress competing pathways [47, 48].  
409 Meanwhile, Mg<sup>2+</sup> is known to support carbohydrate-metabolizing enzymes and the activity of cellulose  
410 synthase regulated by c-di-GMP [49]. Reports on related *Acetobacter* and *Komagataeibacter* strains that  
411 associate Mg<sup>2+</sup> availability with increased BC yield further support this interpretation [50, 51]. Although  
412 these mechanistic links align with previous reports, transcriptomic or metabolomic analyses would be

413 required to confirm these pathways in *K. rhaeticus* SLAM-JS1B. The BBD-derived model captured both  
414 curvature and interaction terms, enabling interpolation within the experimental domain and yielding  
415 predictions that closely matched the validation experiments (prediction accuracy approximately 92%). This  
416 approach enables informed fine-tuning of medium composition without reliance on trial and error. Since all  
417 experiments were conducted under static flask conditions, translating these findings to bioreactor systems  
418 will require adaptation to controlled pH and oxygenation, as well as evaluations of batch reproducibility  
419 and scale-up robustness. The trends observed during preliminary screening were consistent with general  
420 metabolic expectations and previous reports. Glucose outperformed other carbon sources, likely reflecting  
421 its efficient entry into glycolysis and enhanced precursor availability for cellulose biosynthesis [52, 53].  
422 Interestingly, mannitol's performance is compatible with slower catabolism and reduced byproduct  
423 formation [54], whereas lactose yielded the lowest BC titers, likely reflecting limited capacity to hydrolyze  
424  $\beta$ -1,4-glycosidic bonds without specific hydrolases [55, 56]. Among nitrogen sources, complex nitrogen  
425 sources (yeast extract, peptone, tryptone) supported higher production, consistent with their provision of  
426 amino acids, vitamins, and cofactors that benefit growth and cellulose synthesis [57], whereas inorganic  
427 sources performed poorly and ammonium sulfate failed to support detectable synthesis, in line with earlier  
428 observations [52, 58, 59]. Other variables, such as glucose concentration,  $\text{KH}_2\text{PO}_4$ , and incubation time,  
429 showed relatively minor effects within the tested ranges. Temperature profiling further confirmed 25 °C as  
430 optimal, with BC production ceasing at 15 °C and 35 °C, consistent with the mesophilic nature of  
431 *Komagataeibacter* and the temperature sensitivity of cellulose biosynthetic pathways [60, 61].

432 Structural and physicochemical characterization of the BC confirmed that the cellulose produced under  
433 the optimized conditions exhibits the chemical signatures and nanoscale morphology typical of high-purity  
434 BC. The FT-IR spectra exhibited cellulose-specific absorption bands near 3340, 2900, 1430, and 1060  $\text{cm}^{-1}$   
435 [62], and the absence of lignin- or hemicellulose-associated peaks indicated high purity [63]. FE-SEM  
436 analysis revealed a dense, randomly oriented nanofibrillar network with fiber diameters ranging from 50 to  
437 200 nm, consistent with reported morphologies of high-quality *Komagataeibacter*-derived BC. [64]. To  
438 evaluate its functional properties, we immobilized lytic phages targeting *S. Typhimurium* onto the BC

439 matrix [65-67]. *S. Typhimurium* is a major enteric pathogen affecting a wide range of livestock species,  
440 including ruminants such as cattle, sheep, and goats, and it has been frequently isolated from their intestinal  
441 tracts [68, 69]. In particular, infection in young or immunocompromised animals can result in acute enteritis,  
442 dehydration, and growth retardation, underscoring the pathogen's significant impact on animal health and  
443 productivity [70, 71]. Therefore, beyond its role as a dietary fiber comparable to conventional roughage,  
444 phage-BC offers preventive potential against enteric diseases in livestock.

445 Electron micrographs confirmed the successful attachment of *S. Typhimurium* phages to the BC  
446 nanofibrillar network, while antimicrobial assays showed that phages immobilized within BC retained  
447 infectivity against the pathogen. These findings indicate that BC can serve as a biocompatible, structurally  
448 stable delivery matrix for bioactive agents [72]. The antimicrobial efficacy of phage-BC against *S.*  
449 *Typhimurium* suggests potential to reduce pathogen load in livestock, thereby improving gut health, feed  
450 efficiency, and overall production performance while reducing reliance on conventional antibiotics [14].  
451 Given its physicochemical properties and compatibility with phage immobilization, BC may be a promising  
452 carrier for antimicrobial delivery in livestock applications, particularly for targeted interventions in animal  
453 production systems [73-76].

454 Taken together, the sequential and statistically grounded strategy (OVAT, followed by PBD and BBD)  
455 enabled the rational identification of key medium components, defined their optimal levels, and  
456 significantly enhanced BC yields without compromising material quality. This integrative approach  
457 provides a robust framework for strain-specific optimization of culture conditions and establishes a  
458 foundation for downstream studies on large-scale production, cost modeling, and the functional deployment  
459 of BC in antimicrobial applications within the animal industry.

460

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**Table 1. Experimental levels of six variables tested by Plackett–Burman design (PBD) for optimizing BC production from *Komagataeibacter rhaeticus* SLAM-JS1B**

Trails	Variables*						Response
	Glucose (X <sub>1</sub> )	Yeast extract (X <sub>2</sub> )	KH <sub>2</sub> PO <sub>4</sub> (X <sub>3</sub> )	MgSO <sub>4</sub> (X <sub>4</sub> )	Ethanol (X <sub>5</sub> )	Incubation Time (X <sub>6</sub> )	BC (g/L)
1	1(20)	-1(10)	1(5)	-1(1)	-1(0)	-1(8)	0.725
2	1(20)	1(20)	-1(1)	1(2)	-1(0)	-1(8)	0.790
3	-1(10)	1(20)	1(5)	-1(1)	1(10)	-1(8)	1.430
4	1(20)	-1(10)	1(5)	1(2)	-1(0)	1(14)	1.005
5	1(20)	1(20)	-1(1)	1(2)	1(10)	-1(8)	2.270
6	1(20)	1(20)	1(5)	-1(1)	1(10)	1(14)	1.781
7	-1(10)	1(20)	1(5)	1(2)	-1(0)	1(14)	0.776
8	-1(10)	-1(10)	1(5)	1(2)	1(10)	-1(8)	2.149
9	-1(10)	-1(10)	-1(1)	1(2)	1(10)	1(14)	2.272
10	1(20)	-1(10)	-1(1)	-1(1)	1(10)	1(14)	1.881
11	-1(10)	1(20)	-1(1)	-1(1)	-1(0)	1(14)	0.513
12	-1(10)	-1(10)	-1(1)	-1(1)	-1(0)	-1(8)	0.666

Variables\*: X<sub>1</sub>–X<sub>6</sub> (variable); the coded low and high level are presented as – 1 and 1, respectively. Variable levels are presented between brackets expressed as g/L for X<sub>1</sub>–X<sub>4</sub>; ml for X<sub>5</sub>; and days for X<sub>6</sub>.

**Table 2. Experimental levels of three variables tested by Box–Behnken design (BBD) for optimizing BC production from *Komagataeibacter rhaeticus* SLAM-JS1B**

Trails	Variables*			Response
	Yeast extract (X <sub>1</sub> )	MgSO <sub>4</sub> (X <sub>2</sub> )	Ethanol (X <sub>3</sub> )	BC (g/L)
1	-1(10)	-1(1)	0(5)	0.480
2	1(20)	-1(1)	0(5)	0.574
3	-1(10)	1(2)	0(5)	0.523
4	1(20)	1(2)	0(5)	0.605
5	-1(10)	0(1.5)	-1(0)	0.092
6	1(20)	0(1.5)	-1(0)	0.136
7	-1(10)	0(1.5)	1(10)	1.231
8	1(20)	0(1.5)	1(10)	0.968
9	0(15)	-1(1)	-1(0)	0.120
10	0(15)	1(2)	-1(0)	0.137
11	0(15)	-1(1)	1(10)	0.952
12	0(15)	1(2)	1(10)	1.196
13	0(15)	0(1.5)	0(5)	0.528
14	0(15)	0(1.5)	0(5)	0.473
15	0(15)	0(1.5)	0(5)	0.508

Variables\*: X<sub>1</sub>–X<sub>3</sub> (variable); the coded low and high level are presented as – 1 and 1, respectively. Variable levels are presented between brackets expressed as g/L for X<sub>1</sub> and X<sub>2</sub>; ml for X<sub>3</sub>.

## Figure legends

**Figure 1. Isolation of bacterial cellulose-producing strains from Kombucha.** (A) Representative images of BC pellicles formed by *Komagataeibacter intermedius* SLAM-NK6B, *K. rhaeticus* SLAM-JS1B, and *K. rhaeticus* SLAM-JS2B after static aerobic cultivation at 25 °C in GYM medium. (B) Comparison of BC yields determined by the dry weight of freeze-dried pellicles. *K. rhaeticus* strains exhibited significantly higher BC production than *K. intermedius*. Among them, *K. rhaeticus* SLAM-JS1B demonstrated the highest productivity ( $120.8 \pm 28.3$  mg/L) and was selected for subsequent optimization studies. Error bars represent SD of triplicate experiments. (C) Circular whole-genome map of *K. rhaeticus* SLAM-JS1B showing co-localized *bcsB/bcsC* (394,990–401,545), a distal *bcsB* (769,280–770,182), and a GT2 gene (1,908,247–1,908,963). Inner track shows GC content. Whole-genome plots in (B–C) were generated with Proksee. (D) Bacterial cellulose yield (mg/L; dry weight of freeze-dried pellicles) for the three strains cultivated statically at 25°C in GYM medium. Bars indicate mean  $\pm$  SD (n = 3): SLAM-NK6B,  $36.3 \pm 5.3$ ; SLAM-JS1B,  $120.8 \pm 28.3$ ; SLAM-JS2B,  $113.3 \pm 15.0$ .

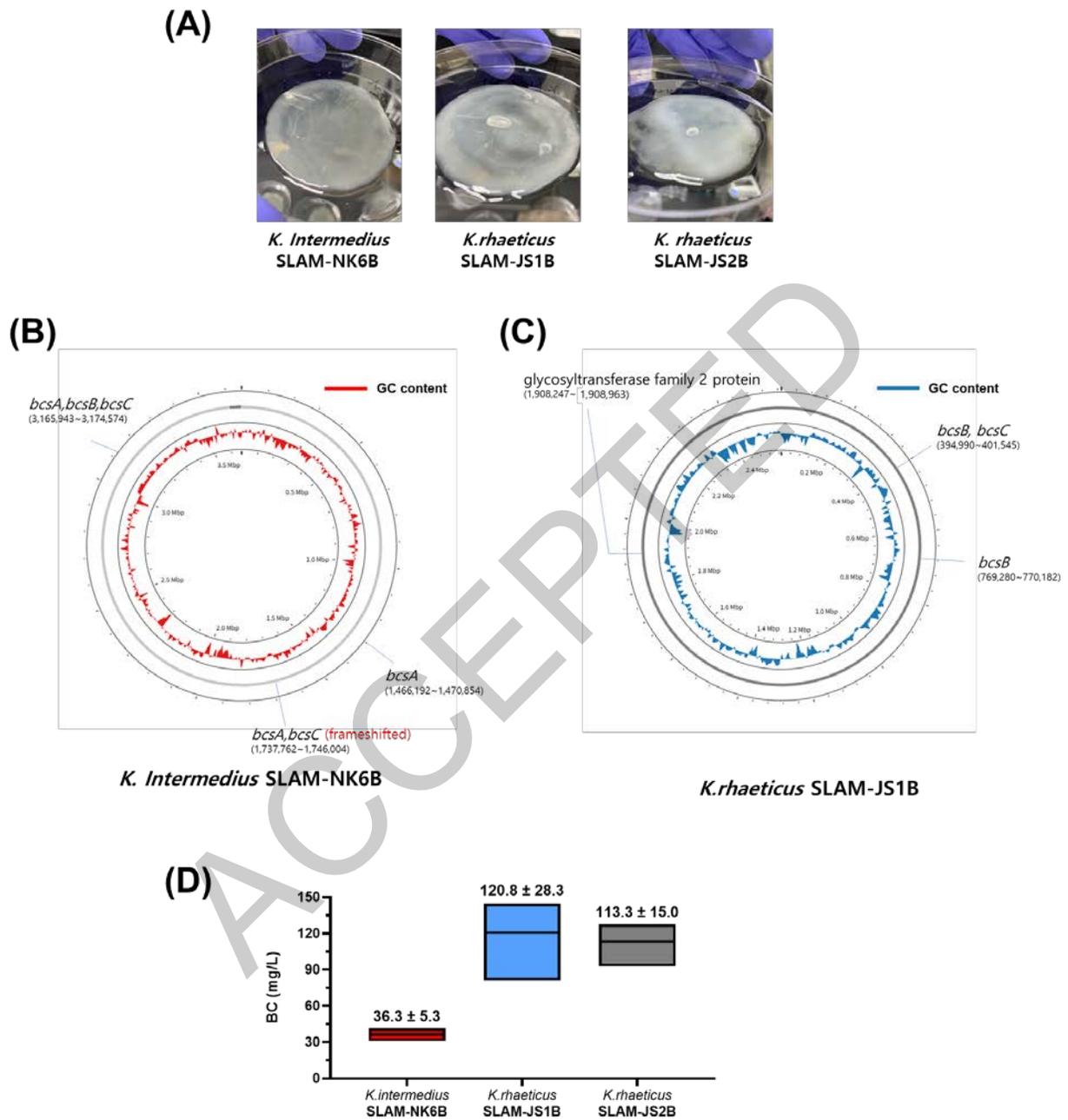
**Figure 2. Screening of medium components and cultivation conditions for BC production by *Komagataeibacter rhaeticus* SLAM-JS1B.** (A) Comparison of BC yields among different basal media (SM, HSM, and GYM). SM exhibited significantly higher productivity than HSM (p = 0.041) and GYM (p = 0.003). (B) Evaluation of carbon sources for BC production. Glucose led to significantly greater yields compared to lactose (p = 0.002) and sorbitol (p = 0.016). (C) Assessment of nitrogen sources revealed that yeast extract significantly outperformed  $\text{NH}_4\text{NO}_3$  (p = 0.0001) and  $\text{NH}_4\text{Cl}$  (p = 0.0006) in supporting BC biosynthesis. (D) Effect of incubation temperature on BC production. The optimal temperature was 25°C, which yielded significantly more BC than 20°C (p = 0.038) and 30°C (p = 0.016). Data are expressed as mean  $\pm$  standard error (SEM). Statistical analysis was performed using unpaired (two-tailed) t-tests, and differences were considered significant at p < 0.05 (\*), p < 0.01 (\*\*), p < 0.001 (\*\*\*), and p < 0.0001 (\*\*\*\*).

**Figure 3. Identification of significant factors affecting *Komagataeibacter rhaeticus* derived BC production using Plackett–Burman Design (PBD).** (A) Main effects plot showing the direct impact of individual variables (each at coded levels of –1 and +1) on BC yield, as defined in Table 1. Positive values indicate a stimulatory effect on BC production, whereas negative values represent inhibitory effects. (B) Pareto chart illustrating the relative contribution of each variable to the overall variability in BC yield. The chart ranks culture components and conditions in descending order of influence, with a cumulative impact accounting for 100% of observed variation.

**Figure 4. Interaction effects of selected medium components on *Komagataeibacter rhaeticus* derived BC biosynthesis using 3D response surface plots of yeast extract, MgSO<sub>4</sub>, and ethanol.** (A) Interaction between yeast extract and MgSO<sub>4</sub>, (B) Interaction between yeast extract and ethanol, (C) Interaction between MgSO<sub>4</sub> and ethanol.

**Figure 5. Structural, physicochemical and morphological comparison between *Komagataeibacter rhaeticus* derived BC and commercial cellulose.** (A) FT-IR spectrum and (B) FE-SEM analysis of BC produced by *K. rhaeticus* and microcrystalline cellulose.

**Figure 6. Phage immobilization on *Komagataeibacter rhaeticus* derived bacterial cellulose (BC) and evaluation of antimicrobial activity.** (A) SEM image of native BC. (B) SEM image of phage–BC (red arrows indicate particle-like features consistent with bound phage). (C) Quantification of immobilized phage density (log particles  $\times$  mm<sup>-2</sup>). (D) Antimicrobial assay with native BC (no inhibition). (E) Antimicrobial assay with phage–BC (distinct lysis zones). (F) Liquid inhibition assay in TSB at 37°C with orbital shaking: growth curves (OD<sub>600</sub>) of native BC (control) and phage–BC (blue). Points are mean  $\pm$  SD (n = 3 technical replicates).



**Fig. 1.**

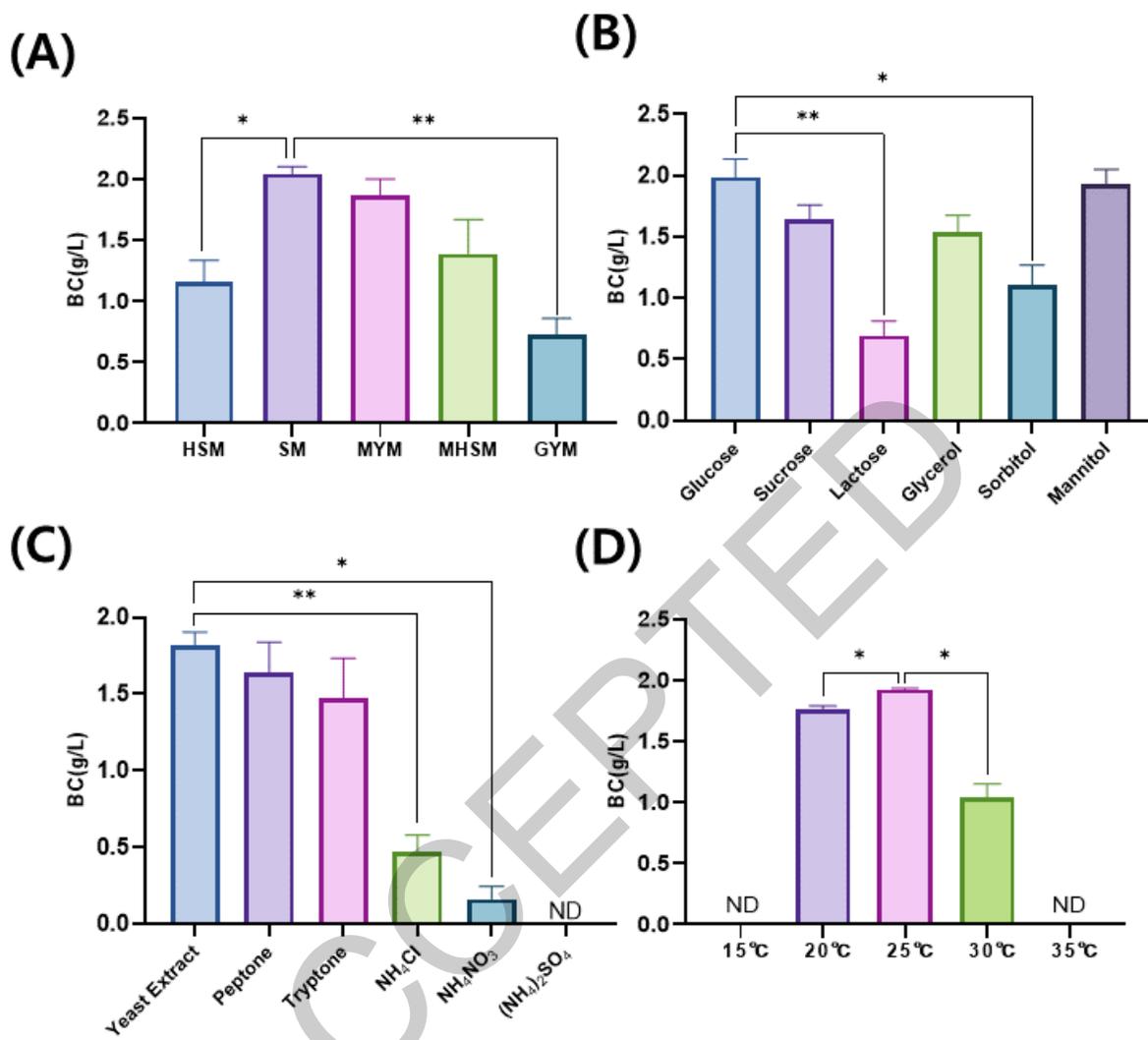


Fig. 2.

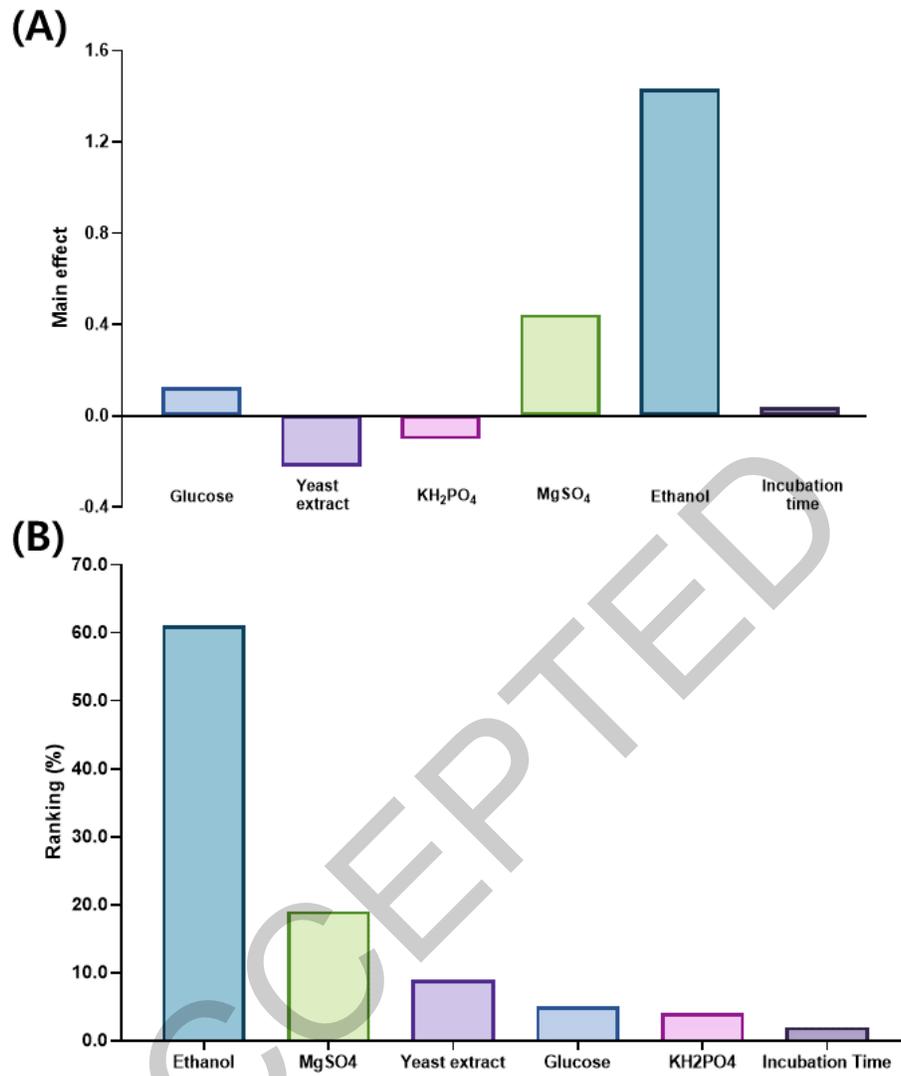


Fig. 3.

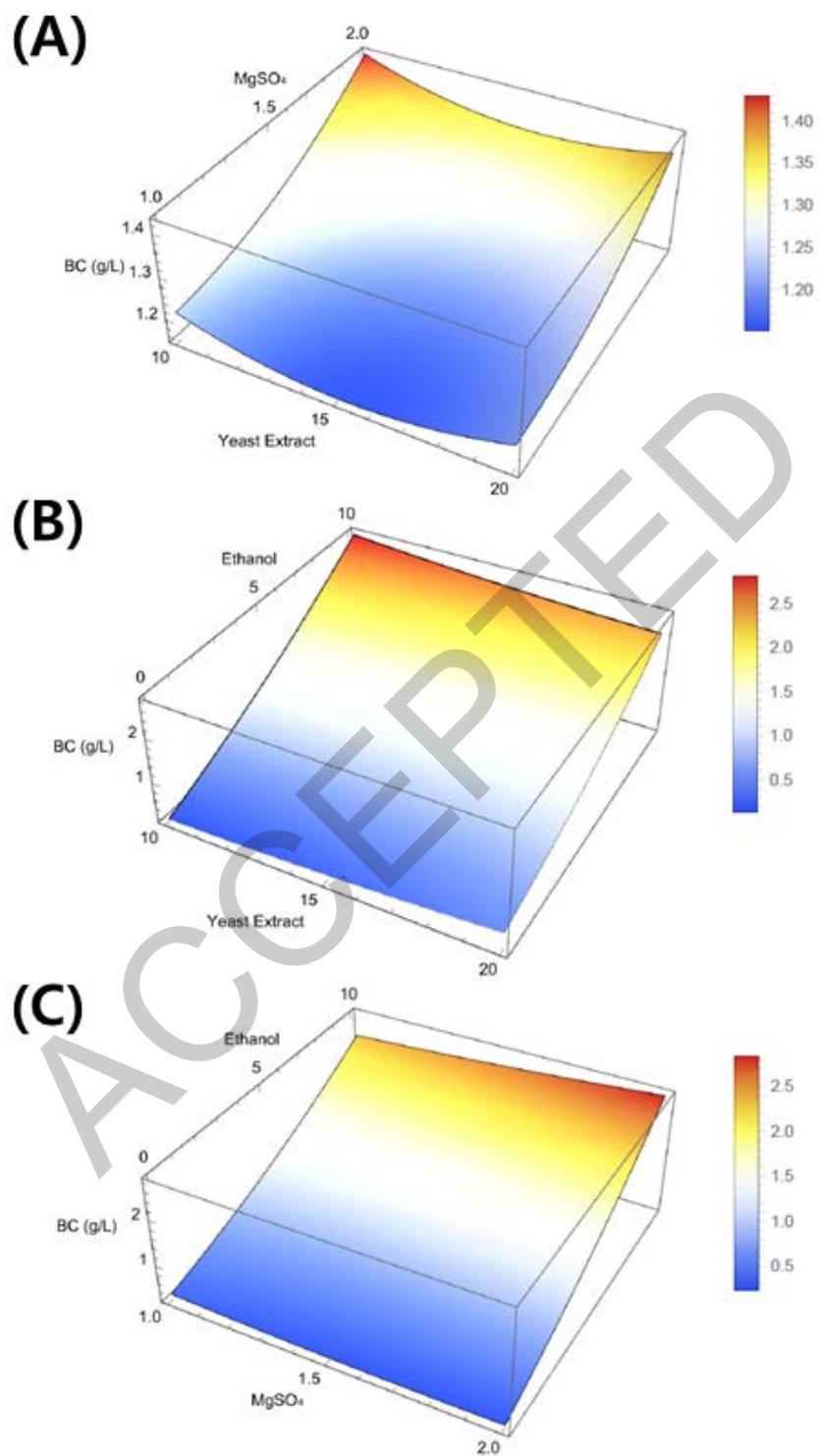


Fig. 4.

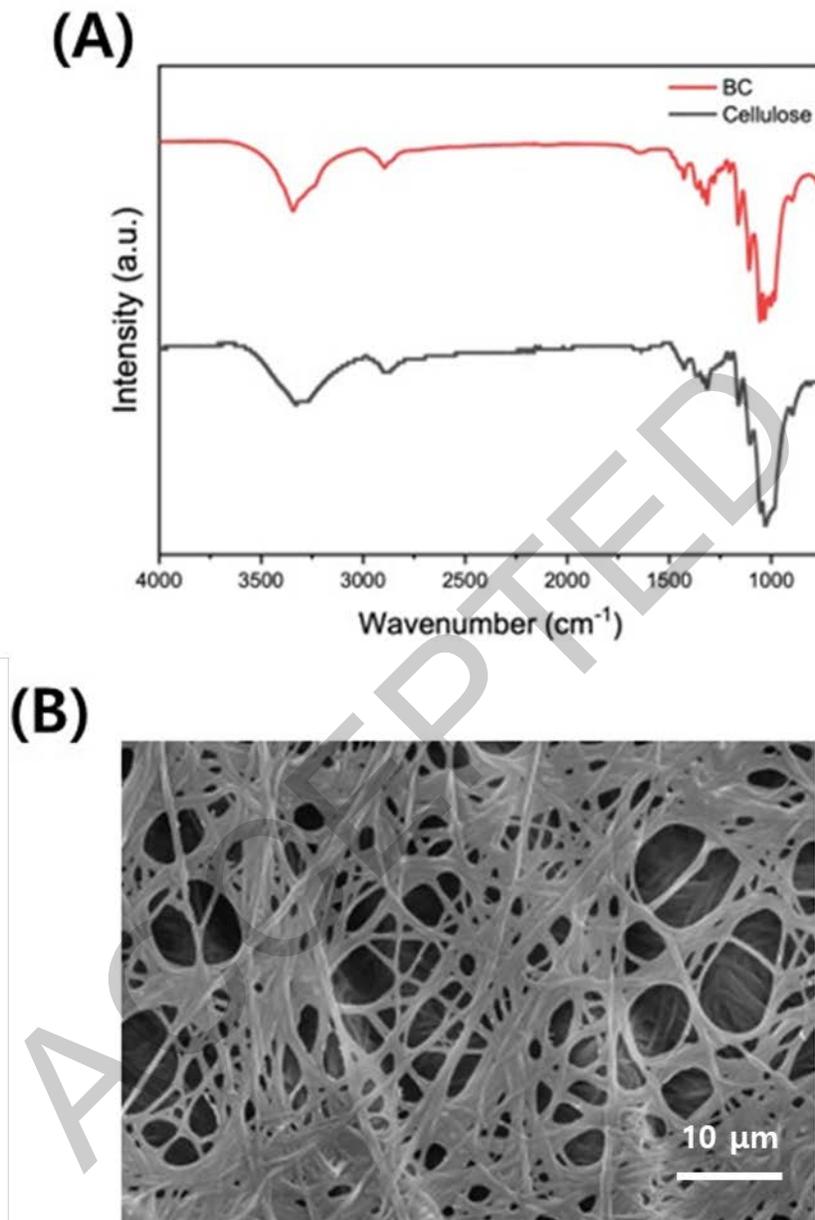


Fig. 5.

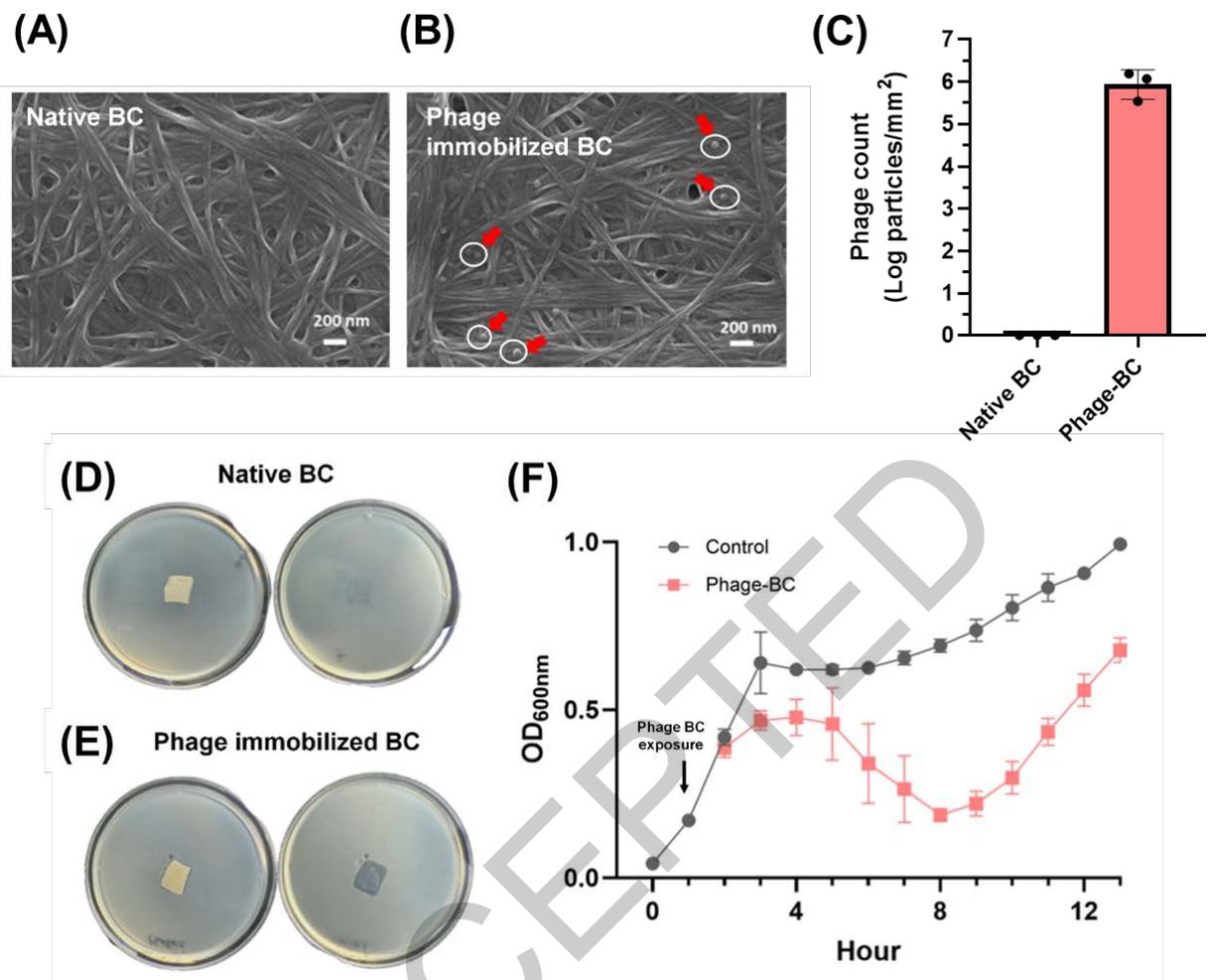


Fig. 6.